

Part of a complete system that incorporates a pilot operated, dome-loaded diaphragm type regulator capable of reducing blanketing gas in a single step, providing bubble-tight shut-off and low maintenance.





GENERAL APPLICATION

The Tank Blanketing System provides a single-source solution to prevent evaporation, reduce fugitive emissions and corrosion, reduce or eliminate combustion potential, prevent contamination or oxidation and provide make-up when the pressure drops in the tank.

TECHNICAL DATA

Connections: $\frac{1}{2}$ ", 1", 2" NPT and

flanged ANSI 150,

300,600

Temperature range: -20 to +300°F

(-29 to +149°C)

Maximum inlet pressure: 200 psig (14 barg) Blanket pressure range: 0.5" wc to 6 psig

(12.7 mm wc to 0.4 barg)

FEATURES

- Single unit system lowers installation costs, reducing labor and materials.
- Simple blanket pressure setting with one unit to calibrate as opposed to conventional multi-unit systems.
- Reduced maintenance costs as top entry provides access to all internal parts without removal from the line.
- Optimum performance reduces supply gas pressure from 200 psig [13.8 barg] to ½" wc [1.2 mbarg] in one stage.
- Balanced design maintains setting accurately regardless of pressure variations.
- O-ring seat and seals assure bubble-tight shut-off.
- Single-source solution provides pad and de-pad valves, regulators, pressure/vacuum vents and low pressure pilot operated valves, emergency vents and valves, flame and detonation flame arresters.
- Combined de-pad and pressure relief valve functions minimizes number of valves and tank connections.
- Component compatibility enables the provision of all major system components in a single tank penetration.

THE NEED FOR EFFECTIVE TANK BLANKETING OR PADDING

Blanketing is a process used to maintain a gas blanket or pad in the vapor space of a pressure-tight liquid storage vessel.

It normally involves the use of a valve or regulator to control the input of the pad gas, usually an inert gas such as nitrogen. When the pressure drops in the tank, the pad or blanketing valve will open and feed gas and pressure into the vessel, limiting the minimum pressure in the tank. This drop in pressure is normally caused by pump out or thermal cooling. In the event of pressure rise in the tank due to heat input or pump in, the de-pad or vent valve will open and vent pressure or pad gas from the tank.

Traditionally, this function was performed by a conservation vent or breather valve. Today, because of the need to collect the gas coming off the top of the tank and prevent the pressure from increasing to a point where the vent valves will leak to atmosphere, a de-pad valve is set to open at a point below the vent valves. Because this valve normally discharges to a closed system, it must be balanced against back pressure.

THE COMPLETE SYSTEM

Because of the interactions between pad (blanketing) valves, de-pad (out breathing) valves, relief devices and flame arresters, each piece of equipment should be considered when specifying the blanketing system and it makes sense to rely on one company to help specify and provide all of the products.

The Tank Blanketing System combines the use of a pilot operated blanketing valve and a pilot operated de-pad valve to provide a simple, reliable and accurate solution. By using a modulating de-pad or vent valve, you can eliminate the need for traditional weight loaded, unbalanced vent valves, reducing project and maintenance costs, conserving blanket gas and further protecting the environment.

Installation flexibility

Depending on your systems needs, the Tank Blanketing System has the flexibility to be installed so that the pad valve, de-pad valve and vacuum breaker can be installed on a single nozzle (Figure 1) or multiple nozzles (Figure 2).

Internal sensing can also be provided in the same tank connection.

Pad valves

BV-1 (flanged)



Type Y1



Type RA



De-pad valves

Type 93



Type 9300



FIGURE 1

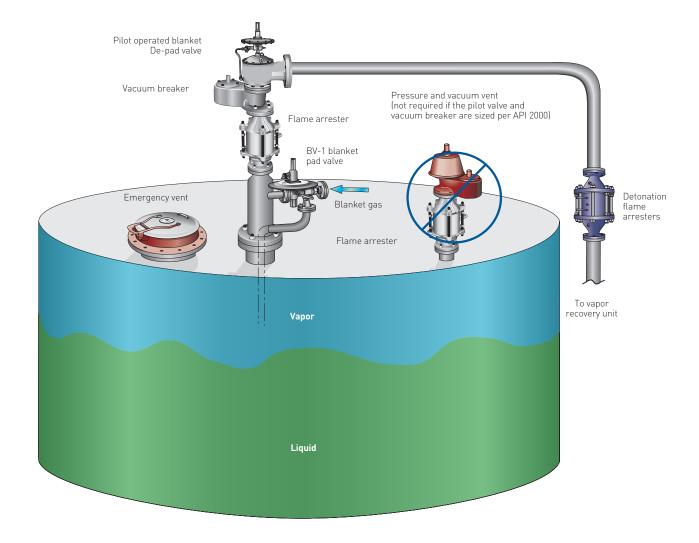
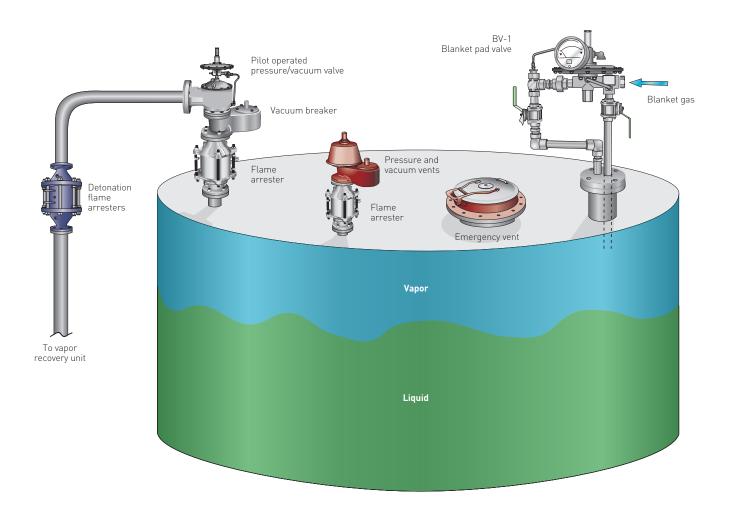


FIGURE 2



SINGLE VALVE SOLUTION

The conventional method (Figure 1) employs as many as four regulators to reduce high supply pressure to low blanket pressures, while the Anderson Greenwood system (Figure 2) requires only one unit to achieve the necessary reduction.

The Type Y1 pilot is used with the main valve to form a pressure reducing valve capable of regulating tank pressures from $\frac{1}{2}$ wc to 6 psig (1.2 mbarg to 0.41 barg).

Type RA direct spring operation

For small flow requirements, the pilot alone can be used as a direct spring tank blanketing valve. The only difference in construction is the location of the sense and inlet ports. The sensed pressure acting against the spring force will determine if the pilot is to open and by how much.

Type Y1 Y-style operation

Upstream pressure enters the main body and acts upward against the main valve diaphragm. Due to a small unbalanced dome area, the effective area above the diaphragm is slightly larger than below. Shut-off will occur when the dome pressure is equal to the inlet pressure. The sleeve/diaphragm retainer assembly is lightly spring loaded to provide initial closing force when there is no pressure differential across the diaphragm.

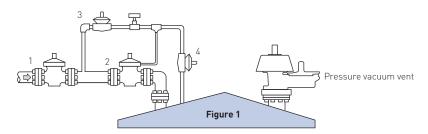
The Type Y1 pilot controls dome pressure in response to tank pressure. A reduction in dome pressure allows the sleeve to move upward off the main seat, permitting flow through the valve. The amount of lift depends on the pressure reduction in the dome: the greater this reduction, the greater the flow.

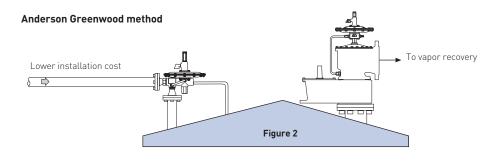
When the downstream pressure is satisfied, the sensed pressure acting on the pilot sense plate will overcome the spring force to close the pilot, which in turn closes the valve. No system fluid is vented to the atmosphere.

Type BV-1 right-angle style operation

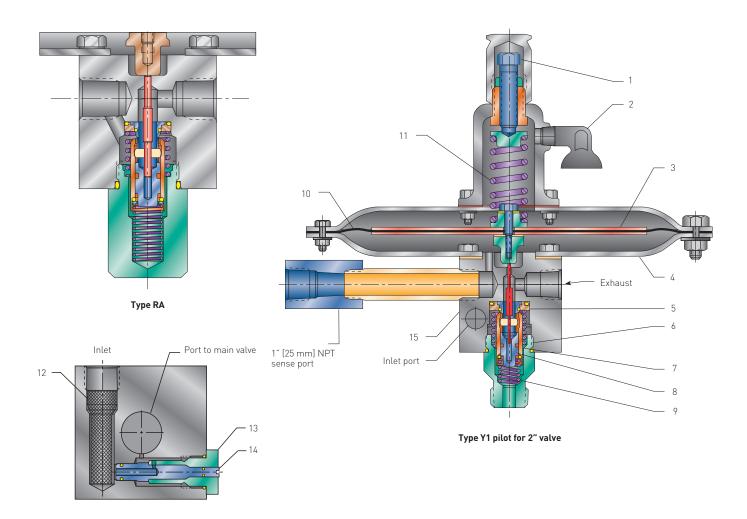
The diaphragm and sleeve are replaced by a piston in the main valve for more rugged construction. As with the Y1 valve, the pilot controls dome pressure. A reduction in dome pressure allows the piston to move horizontally off the seat, permitting flow through the valve. Maximum flow is controlled by the cage orifices.

Conventional method





TYPE RA AND Y1 PILOT MATERIALS OF CONSTRUCTION



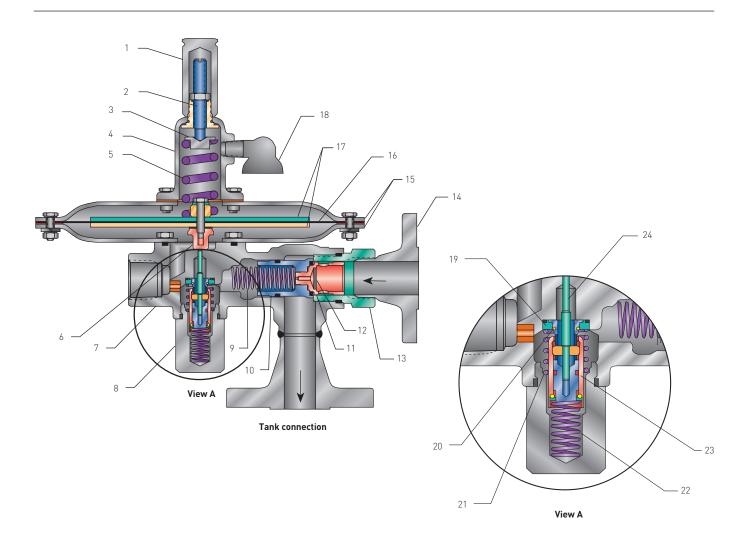
PARTS AND MATERIALS

PARIS	AND MAI ERIALS		
No.	Part name	CS	SS
1	Set pressure adjustment screw	SS 304/CS	SS 304/316
2	Vent	Zytel	Zytel
3	Sense plate	CS 1010/ZNC0	SS 302/304
4	Case	CS A36	SS 304
5	Seat and seals	NBR ¹	NBR ¹
6	Sleeve	SS A479-316	SS A479-316
7	Sleeve seal	NBR ¹	NBR ¹
8	Nozzle - pilot	SS A479-316	SS A479-316
9	Sleeve spring	SS 316	SS 316
10	Diaphragm	NBR ²	NBR ²
11	Set pressure spring	SS 316	SS 316
12	Filter screen	SS 302	SS 302
13	Orifice retainer	SS A479-316	SS A479-316
14	Adjustable orifice core	SS A276-316	SS A276-316
15	Body	CS A108 1018	SS A479 316

NOTES

- 1. NBR standard, FKM, EPR, Kalrez® optional.
- 2. NBR standard, FKM, EPR, PTFE optional.

1" TYPE BV-1 MATERIALS OF CONSTRUCTION

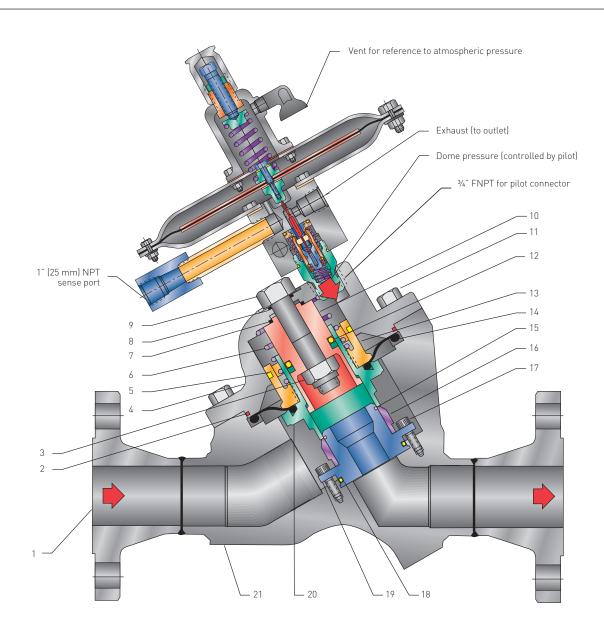


MATERIALS OF CONSTRUCTION

No.	Part name	CS	SS
1	Pilot cap	SS A582-303	SS A582-303
2	Pressure adj. screw	SS A276-304	SS A276-304
3	Spring washer	STL A108-1213	SS A479-316
4	Bonnet assembly	SS SA351-CF8M	SS SA351-CF8M
5	Spring	SS 316	SS 316
6	Actuator	STL 12L14/ZNC0	SS A479-316
7	Body	SS SA351-CF8M/SA105	SS CF8M, SA-182-316
8	Body plug	STL SA108-1018/ZNC0	SS A479-316
9	Piston spring	SS 316	SS 316
10	Piston	SS A479-316	SS A479-316
11	Seat retainer/flow cage	SS A479-316	SS A479-316
12	Screen filter	SS 316	SS 316
13	Bushing nozzle	SS A479-316	SS A479-316
14	Inlet flange	STL SA105	SS SA182-316
15	Case	STL A36	SS A240-304
16	Diaphragm	PTFE	PTFE
17	Sense plate	STL 1010	SS 302/304
18	Vent	Zytel	Zytel
19	Nozzle retainer	SS A479-316	SS A479-316
20	Pilot seat	Fluorosilicone ¹	Fluorosilicone ¹
21	Nozzle retainer spring	SS 316	SS 316
22	Pilot sleeve spring	SS 302	SS 302
23	Pilot sleeve	SS A479-316	SS A479-316
24	Spindle	SS A276-316	SS A276-316

NOTE

^{1.} Fluorosilicone standard, NBR, EPR, Kalrez® optional.



MAIN VALVE

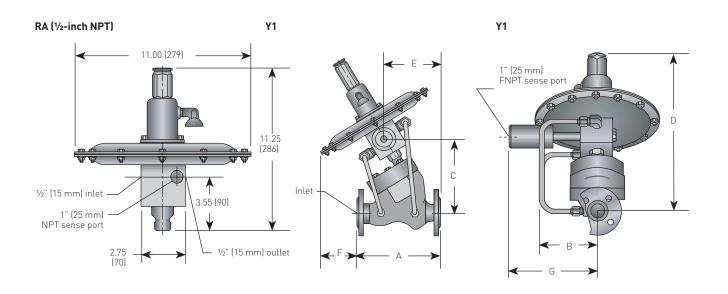
No	Part name	CS	SS
1	Flange	Steel A105	SS 182-316
2	Cap seal	NBR ¹	NBR ¹
3	Lock nut	Alloy steel	SS 18-8
4	Сар	Steel A216-WCB	SS A351-CF8M
5	Ring	SS 316	SS 316
6	Spring	SS 316	SS 316
7	Piston seal	NBR ¹	NBR ¹
8	Seal piston bolt	NBR ¹	NBR ¹
9	Piston bolt	Alloy steel	SS 18-8
10	Piston	SS 303	SS A479-316
11	Cap bolt	Alloy steel	SS 18-8

Part name	CS	SS
Sleeve seal	NBR ¹	NBR ¹
Diaphragm retainer	Steel 1213	SS A479-316
Diaphragm	NBR ¹	NBR ¹
Seat	NBR ¹	NBR ¹
Seat retainer	SS 316	SS 316
Nozzle screw	SS 18-8	SS 18-8
Nozzle seal	NBR ¹	NBR ¹
Nozzle	SS 316	SS 316
Sleeve	Steel A31-8620 ²	SS A479-316 ²
Body	Steel A216-WCB	SS A351-CF8M
	Sleeve seal Diaphragm retainer Diaphragm Seat Seat retainer Nozzle screw Nozzle seal Nozzle Sleeve	Sleeve seal NBR1 Diaphragm retainer Steel 1213 Diaphragm NBR1 Seat NBR1 Seat retainer SS 316 Nozzle screw SS 18-8 Nozzle seal NBR1 Nozzle SS 316 Sleeve Steel A31-86202

NOTES

- 1. NBR standard; FKM, EPR, Kalrez® optional. Kalrez® not available for Item 14.
- 2. Chrome plated.

DIMENSIONS AND WEIGHTS

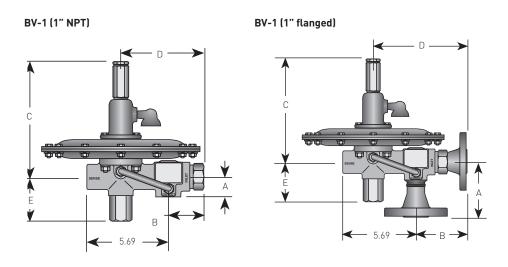


DIMENSIONS, INCHES (mm) AND WEIGHTS, LB (kg)

DIMENSION	DIMENSIONS, INCHES (IIIII) AND WEIGHTS, LB (kg)												
		Di	imension	5			Maximum						
				A flanges	1								
Model	Size	A threaded ends	150#	300#	600#	В	С	D	E	F	G	Weight total	Pilot and cap
Y1	1"	6.75	7.25	7.75	8.25	5.00	7.38	14.50	5.63	3.65	7.13	39	21
	(25)	(171)	(184)	[197]	(210)	[127]	(187)	(368)	(143)	(93)	(181)	(17.69)	(9.52)
Y1	2"	9.19	14.37	14.87	15.62	5.25	10.00	17.00	9.75	2.75	7.13	75	27
	(50)	(233)	(365)	(378)	(397)	(133)	(254)	(432)	(248)	(70)	(181)	(34.0)	(12.3)

NOTE

1. Contact your sales representative for other flange configurations.



DIMENSIONS, INCHES (mm) AND WEIGHTS, LB (kg)

Connection	Α	В	С	D	Е	Weight
Threaded	1.91 (44)	2.53 (64)	8.25 (210)	5.84 (148)	3.25 (83)	18.5 (8.4)
150# flange	4.06 (103)	4.06 (103)	8.25 (210)	7.37 (187)	3.25 (83)	23.5 (10.7)
300# flange	4.31 (109)	4.31 (109)	8.25 (210)	7.62 (193)	3.25 (83)	26.5 (12.0)

Dimensions are $\pm .06$ (± 1.5 mm), unless noted otherwise. For other configurations, contact your sales representative.

PRESSURE/TEMPERATURE RANGE

Set pressure ¹					
½" wc to 1.4" wc	(1.2 to 3.5 mbarg)	0.6 to 1.4 psig	(41 to 97 mbarg)		
1.2" wc to 4" wc	(3.0 to 10.0 mbarg)	1.3 to 3.1 psig	(90 to 215 mbarg)		
3.5" wc to 10" wc	(8.7 to 25 mbarg)	2.3 to 3.5 psig	(160 to 241 mbarg)		
8" wc to 18" wc	(20 to 45 mbarg)	3.0 to 6.0 psig	(207 to 414 mbarg)		
15" wc to 29" wc	(37 to 72 mhard)				

Minimum inlet pressure

RA: No minimum BV-1: 15 psig (1.03 barg) Y1: 30 psig (2.07 barg)

Maximum pressure at sense port2

15 psig (1.03 barg)

Temperature³

-20°F to 300°F [-29°C to 149°C]

NOTES

- 1. For higher set pressures than those published, contact your sales representative.
- 2. High strength cases available to 280 psig (19.3 barg).
- 3. For lower temperatures than those published, contact your sales representative.

PERFORMANCE CHARACTERISTICS

Set pressure is defined as the point at which the valve begins to flow. As the demand for flow increases, the tank pressure must drop in order for the valve to respond, since a differential pressure is required to create the necessary forces to operate the valve.

This drop in tank pressure is called 'droop'. When the valve is 100% open, the tank pressure must increase for the valve to respond and close.

The difference between start to open and close is called 'deadband'. For the Type Y1 blanketing valve, this deadband is 1" wc (2.5 mbarg) at the lowest set pressure. For the Type BV-1 blanketing valve, it is 3/4" wc (1.9 mbarg). Lockup, the rise above set pressure for total closure, is less than 0.1" wc (0.25 mbarg).

Elastomer selection

For diaphragms, seats and seals, it is important to specify an elastomer that is compatible with both the supply gas and the product being stored in the tank, as vapors will enter the valve from the discharge port and sense line. The RA and Y1 valves come with NBR soft goods as standard. The BV1 comes standard with Fluorosilicone and FKM seat and seals and a PTFE diaphragm. It is available with an internal purge which sweeps a small flow rate of blanket gas back through the sense port and tank connection.

NACE trim

Pilot and main valve trims are available for sour gas service in accordance with the latest edition of NACE MR0175.

GOX/LOX

The BV-1 model can be cleaned for GOX and LOX applications.

SIZING

When sizing for tank blanketing, it is imperative to consider both:

- a. blanketing gas replacement for liquid loss during pump-out
- b. the condensation/contraction of tank vapors during atmospheric thermal cooling.

The required amount of blanketing gas and correct size of valve must be determined on the basis that both conditions could occur simultaneously.

The maximum flow rate through the blanketing valve will determine the size of relief valve. If a flow rate less than that listed in table C is required, restricted nozzles are available to limit the flow to 70, 50, 30 or 10% of the 100% rated capacity. Where applicable, the use of restricted nozzles will minimize the size of safety relief valve required. The BV-1 is also available with a 110% piston for increased capacity.

To size a blanketing valve

- 1. Determine the gas flow rate due to pump-out (from Table A).
- 2. Determine the gas flow rate due to atmospheric thermal cooling (from Table B).
- 3. Add the requirements of 1 and 2 and select valve size based on air capacity (from Table C).

Excerpt from API 20001

For tanks with a capacity of 20 000 bbl or more, the requirements for the vacuum condition are very close to the theoretically computed value of 2 SCFH of air, per square foot of total shell and roof area.

For tanks with a capacity of less than 20 000 bbl, the requirements for the vacuum condition have been based on 1 SCFH of air for each barrel of tank capacity. Substantially, this is equivalent to a 100°F (38°C) per hour mean rate of vapor space temperature change (see Table B).

NOTE

1. API 2000, Section 2.4, Table 2.

GAS FORMULA

VALUES C ₂ AND G					
Gas	C_2	G			
Air	1.00	1.00			
Natural gas	0.98	0.60			
Nitrogen	1.00	0.97			

English units

$$V = 907 C_2 C_V P_1 \sqrt{\frac{X}{GT}}$$

Metric units

$$V = 263 C_2 C_V P_1 \sqrt{\frac{X}{GT}}$$

C_v VALVE SIZING COEFFICIENTS

Valve s	size	Nozzle size	C _v
RA:	½" (15 mm)	No options	0.385
BV-1:	1" (25 mm)	110%	14.5
BV-1:	1" (25 mm)	100%	13.2
BV-1:	1" (25 mm)	70%	9.2
BV-1:	1" (25 mm)	50%	6.6
BV-1:	1" (25 mm)	30%	4.0
BV-1:	1" (25 mm)	20%	2.6
BV-1:	1" (25 mm)	10%	1.3
BV-1:	1" (25 mm)	5%	0.7
Y1:	1" (25 mm)	100%	10.0
Y1:	1" (25 mm)	70%	7.0
Y1:	1" (25 mm)	50%	5.0
Y1:	1" (25 mm)	30%	3.0
Y1:	2" (50 mm)	100%	43.6
Y1:	2" (50 mm)	70%	30.5
Y1:	2" (50 mm)	50%	21.8
Y1:	2" (50 mm)	30%	13.1
Y1:	2" (50 mm)	10%	4.4

NOMENCLATURE

Symbol	Description	English units	Metric units
V	Required capacity	SCFM	Nm³/hr
C_2	Correction factor for specific heat ratio	-	-
C_{v}	Valve sizing coefficient	-	-
P_1	Supply pressure at valve	psia	bara
X	0.66 for $P_1 \le$ 0.69 for $P_1 >$	47.7 psia	3.288 bara
G	Specific gravity	-	-
Т	Relieving temperature	°R (°F + 460)	°K (°C + 273)

SIZING DATA

TABLE A (English) - in breathing rate due to pump-out

Multiply maximum pump-out rate in:	Ву	To obtain
U.S. GPM	8.021	SCFH air required
U.S. GPH	0.134	SCFH air required
Barrels/hr	5.615	SCFH air required
Barrels/day	0.234	SCFH air required
Liters/min	2.118	SCFH air required
m ³ /hr	35.300	SCFH air required

TABLE A (Metric) - in breathing rate due to pump-out

···					
Multiply maximum pump-out rate in:	Ву	To obtain			
U.S. GPM	0.215	Nm ³ /hr air required			
IMP GPM	0.258	Nm ³ /hr air required			
Barrels/hr	0.151	Nm ³ /hr air required			
Barrels/day	0.0063	Nm ³ /hr air required			
Liters/min	0.057	Nm ³ /hr air required			

TABLE B¹ - in breathing rate due to thermal cooling

TABLE B ¹ - in breathing rate due to thermal cooling Tank capacity In breathing air							
Required barrels	Gallons	(m ³)	SCFH	(Nm³/hr)			
60	2500	(9.5)	60	(1.6)			
100	4200	(15.9)	100	(2.7)			
500	21 000	(79.5)	500	(13.4)			
1000	42 000	(159)	1000	(26.8)			
2000	84 000	(318)	2000	(53.6)			
3000	126 000	(477)	3000	(80.4)			
4000	168 000	(636)	4000	(107.2)			
5000	210 000	(795)	5000	(134)			
10 000	420 000	(1590)	10 000	(268)			
15 000	630 000	(2385)	15 000	(402)			
20 000	840 000	(3180)	20 000	(536)			
25 000	1 050 000	(3975)	24 000	(643)			
30 000	1 260 000	(4770)	28 000	(750)			
35 000	1,470 000	(5560)	31 000	(830)			
40 000	1 680 000	(6360)	34 000	(911)			
45 000	1 890 000	(7150)	37 000	(992)			
50 000	2 100 000	(7950)	40 000	(1070)			
60 000	2 520 000	(9540)	44 000	(1180)			
70 000	2 940 000	(11130)	48 000	(1290)			
80 000	3 360 000	(12700)	52 000	(1400)			
90 000	3 780 000	(14300)	56 000	(1500)			
100 000	4 200 000	(15900)	60 000	(1600)			
120 000	5 040 000	(19100)	68 000	(1800)			
140 000	5 880 000	(22300)	75 000	(2000)			
160 000	6 720 000	(25400)	82 000	(2200)			
180 000	7 560 000	(28600)	90 000	(2400)			

NOTE

1. API 2000, Section 2.4, Table 2.

TABLE C (English) - Flow capacities in SCFH at $60^{\circ}F^{1}$ gas temperature, 100% nozzle

		Type RA, ½"		BV-1, 1"			Y1, 1"			Y1, 2"			
Inlet pressure	Outlet	Natural			Natural			Natural			Natural		
(psig)	press.*	gas	Nitrogen	Air	gas	Nitrogen	Air	gas	Nitrogen	Air	gas	Nitrogen	Air
15		468	375	369	16027	12862	12688	-	-	-	-	-	-
20		547	439	432	18725	15028	14801	-	-	-	-	-	-
25		625	502	494	21424	17193	16933	-	-	-	-	-	-
30		704	565	556	24122	19359	19066	18274	14666	14444	79675	63942	62975
40		880	706	696	30182	24222	23856	22865	18350	18072	99691	80005	78796
50		1042	835	823	35699	28650	28217	27045	21704	21376	117916	94631	93201
60		1203	966	951	41217	33078	32578	31225	25059	24680	136141	109258	107606
70		1363	1095	1078	46735	37506	36939	35405	28414	27984	154366	123884	122011
80		1525	1224	1205	52252	41934	41300	39585	31768	31288	172591	138510	136416
90		1685	1353	1333	57770	46362	45662	43765	35123	34592	190816	153136	150822
100		1847	1482	1460	63288	50790	50023	47945	38478	37896	209041	167762	165227
110		2008	1611	1587	68805	55219	54384	52125	41832	41200	227266	182388	179632
120		2168	1740	1713	74323	59647	58745	56305	45187	44504	245491	197015	194037
130		2330	1870	1841	79840	64075	63106	60485	48541	47808	263715	211641	208442
140		2490	1999	1968	85358	68503	67467	64665	51896	51112	281940	226267	222847
150		2651	2128	2095	90876	72931	71829	68845	55251	54416	300165	240893	237252
160		2813	2257	2223	96393	77359	76190	73025	58605	57720	318390	255519	251657
170		2973	2386	2350	101911	81787	80551	77205	61960	61023	336615	270145	266062
180		3135	2515	2477	107429	86215	84912	81385	65315	64327	354840	284772	280468
190		3296	2644	2605	112946	90643	89273	85565	68669	67631	373065	299398	294873
200		3456	2773	2732	118464	95071	93635	89745	72024	70935	391290	314024	309278

^{* 1} psig or less

TABLE D - CORRECTION FACTORS

Actual temperature °F	Correction factor
-20	1.0870
0	1.0630
20	1.0410
40	1.0200
60	1.0000
80	0.9813
100	0.9636
120	0.9469
150	0.9233
200	0.8876
250	0.8558

NOTE

To obtain capacities at a temperature other than 60°F, multiply capacity in Table C by appropriate temperature correction factor in Table D.

TABLE C (metric) - Flow capacities in Nm 3 /hr at 0°C 1 gas temperature, 100% nozzle

		Type RA, ½" (15 mm)			BV-1, 1" (25 mm)			Y1, 1" (25 mm)			Y1, 2" (50 mm)		
Inlet pressure	Outlet	Natural			Natural			Natural			Natural		
(barg)	press.*	gas	Nitrogen	Air	gas	Nitrogen	Air	gas	Nitrogen	Air	gas	Nitrogen	Air
1.0		13	10	10	435	349	344	-	-	-	-	-	-
2.0		19	15	15	651	522	514	493	396	390	-	-	-
3.0		26	21	20	886	711	700	671	539	531	2927	2349	2313
4.0		32	26	26	1107	888	875	839	673	663	3656	2934	2890
5.0		39	31	31	1328	1066	1049	1006	807	795	4386	3520	3466
6.0		45	36	36	1549	1243	1224	1173	941	927	5115	4105	4043
7.0		52	41	41	1769	1420	1399	1340	1076	1059	5844	4690	4619
8.0		58	47	46	1990	1597	1573	1508	1210	1192	6574	5276	5196
9.0		64	52	51	2211	1774	1748	1675	1344	1324	7303	5861	5772
10.0		71	57	56	2432	1952	1922	1842	1478	1456	8032	6446	6349
11.0		77	62	61	2653	2129	2097	2010	1613	1588	8762	7032	6925
12.0		84	67	66	2873	2306	2271	2177	1747	1721	9491	7617	7502
13.0		90	72	71	3094	2483	2446	2344	1881	1853	10220	8202	8078
14.0		97	78	76	3315	2660	2620	2511	2015	1985	10950	8788	8655

^{* 70} mbarg or less

TABLE D - CORRECTION FACTORS

TABLE D - CONNECTION TACTORS								
Actual temperature (°C)	Correction factor							
(-30)	1.060							
(-20)	1.039							
(-10)	1.019							
(0)	1.000							
(10)	0.982							
(20)	0.965							
(30)	0.949							
(40)	0.934							
(50)	0.919							
(100)	0.855							
(150)	0.803							

NOTE

To obtain capacities at a temperature other than
 O°C, multiply capacity in Table C by appropriate
 temperature correction factor in Table D.

SELECTION GUIDE Y1R Example: Basic valve type **BV** Right angle style - pilot operated Y1R Y style - pilot operated RAR Direct spring Valve size 1" (25 mm) (BV-1 or Y1) 1 2 2" (50 mm) (Y1 only) 5 ½" (15 mm) FNPT (RA only) Connections s Threaded (internal NPT) PN 6 PN 10/16 1 150# М 300# PN 25/40 3 Ν Nozzle/piston1 100 percent 3 30 percent 5 percent (BV-1 only) 20 percent (BV-1 only) 7 70 percent 2 110 percent (BV-1 only) 5 50 percent 10 percent **Body material** CS (RA and Y1 only) s 316 SS CS/NACE (All SS in BV-1, RA models) Ν Main valve trim material Standard trim 2 316 SS trim (RA, BV-1 standard) Seat, seal, and diaphragm material В NBR (RA, Y1 standard) ٧ FKM EPR Ε Х Other (specify) Fluorosilicone with PTFE pilot diaphragm (standard for BV-1 model only) Set pressure range 0.6 psig to 1.4 psig (41 to 97 mbarg) 1 ½" wc to 1.4" wc (1.2 to 3.5 mbarg) 6 1.3 psig to 3.1 psig (90 to 215 mbarg) 2 1.2" wc to 4" wc (3.0 to 10.0 mbarg) 7 3 3.5" wc to 10" wc (8.7 to 25 mbarg) 8 2.3 psig to 3.5 psig (160 to 240 mbarg) 4 8" wc to 18" wc (20 to 45 mbarg) 3.0 psig to 6.0 psig (0.2 to 0.41 mbarg) 15" wc to 29" wc (37 to 72 mbarg) 5 **Options** Υ Pilot filter (available Y1 only) Ν No options Ε External purge meter

- Ρ Internal purge (available BV-1 only)
- s Sense line control gauge
- Т System pressure gauge
- Both sense line gauge and tank pressure gauge

For special requirements contact your sales representative.

NOTE

1. RA is always 100 percent.